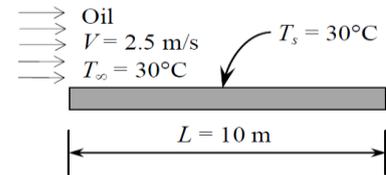


## In-Class Exercises n°03

### Exercise 3.1

Engine oil at  $80^\circ\text{C}$  flows over a **10-m-long** flat plate whose temperature is  $30^\circ\text{C}$  with a velocity of **2.5 m/s**. Determine the **total drag force** ( $F_D$ ) and the **rate of heat transfer** ( $q_v$ ) over the entire plate per unit width.



(Figure 3.1)

### Exercise 3.2

Hydrogen at  $15^\circ\text{C}$  and a pressure of **1 atm** is flowing along a flat plate at a velocity of **3 m/s**. If the plate is **0.3 m** wide and at  $71^\circ\text{C}$ ,

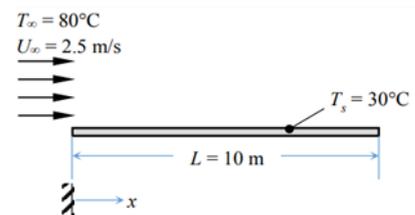
- 1) Determine the regime flow of hydrogen over the flat plate?
- 2) Sketch a representative scheme.

**Calculate** the following quantities at  $x = 0.3\text{ m}$ :

- 3) hydrodynamic boundary layer thickness ( $\delta$ ), in **cm**,
- 4) thickness of thermal boundary layer ( $\delta_T$ ), in **cm**,
- 5) local friction coefficient ( $C_{f,x}$ ), dimensionless,
- 6) average friction coefficient ( $\overline{C_f}$ ), dimensionless,
- 7) drag force ( $F_D$ ), in **N**,
- 8) local convection heat transfer coefficient ( $h_x$ ), in **W/m<sup>2</sup>·K**,
- 9) average convection heat transfer coefficient ( $\overline{h}$ ), in **W/m<sup>2</sup>·K**, and
- 10) rate of heat transfer ( $q$ ), in **W**.

### Exercise 3.3

A new heat transfer fluid called *ThermoKool* ( $k = 0.1414\text{ W/m}\cdot^\circ\text{C}$ ,  $\rho = 867\text{ kg/m}^3$ ,  $\mu = 0.06108\text{ kg/m}\cdot\text{s}$ ,  $Pr = 1551$ ) flows over a flat plate with a velocity of  $U_\infty = 2.5\text{ m/s}$  and temperature  $T_\infty = 80^\circ\text{C}$ . The plate is maintained at  $T_s = 30^\circ\text{C}$ . Dimensions are shown in the figure.



- 1) Determine if the flow is entirely laminar, entirely turbulent, or whether it transitions somewhere along the plate.
- 2) Find the total rate of heat transfer per unit width from the *ThermoKool* to the plate.

Correlation	Geometry	Conditions
$Nu_x = 0,332 \cdot Re^{1/2} \cdot Pr^{1/3}$	Flat plate	local, laminar ; $Pr \geq 0.6$
$Nu_L = 0,664 \cdot Re_L^{1/2} \cdot Pr^{1/3}$		average, laminar ; $Pr \geq 0.6$
$Nu_x = 0,0296 \cdot Re^{0.8} \cdot Pr^{1/3}$		local, turbulent ; $100 > Pr > 0.6$ , $Re_x > 500\ 000$
$Nu_L = 0,037 \cdot Re_L^{0.8} \cdot Pr^{1/3}$		average, turbulent ; $100 > Pr > 0.6$ ; $Re_L > 500\ 000$
$\overline{Nu_L} = (0,037 \cdot Re_L^{0.8} - 871) \cdot Pr^{1/3}$		average, mixed ; $100 > Pr > 0.6$ , $Re_{x,cr} = 500\ 000$ ; $Re_L \leq 10^8$ ; $0,6 \leq Pr \leq 60$